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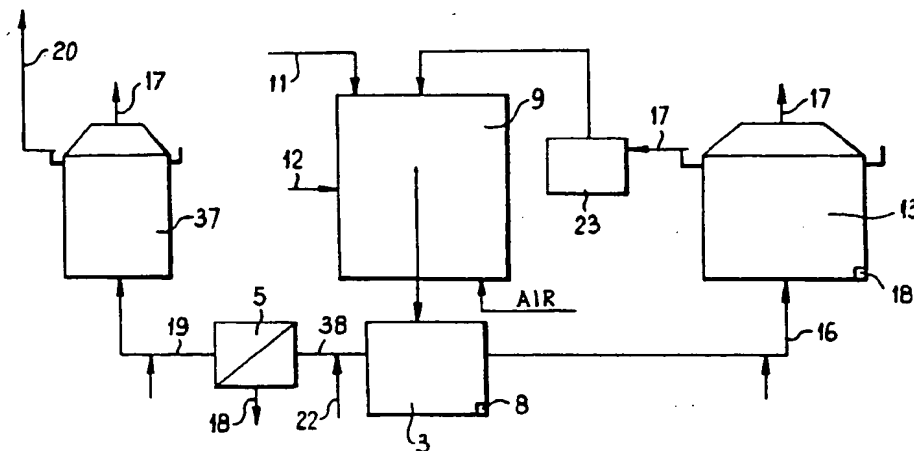
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(54) Method and apparatus for processing manure.

(57) The invention relates to a method for processing manure, liquid manure and/or Kjeldahl-N containing waste water being subjected to a nitrification in an aerated reactor containing active sludge and to a denitrification in a high rate denitrification reactor (13) containing a very compact biomass capable of converting nitrate to nitrogen gas. The loading of the nitrification reactor (9) being controlled to obtain an optimum nitrification and denitrification, the effluent from the nitrification reactor (9) partial being passed to the denitrification reactor (13), adding a source of carbon to the effluent to be passed to the denitrification reactor (13) and passing an other portion of the effluent stream from the nitrification reactor (9) to a separation step (5) to separate a sludge (18) the effluent from separation step (5) being passed to a denitrification reactor (37) under the addition of a carbon source if desired. The invention further relates to an apparatus constructed for this purpose.

fig - 11



The present invention relates to a method for processing manure, liquid manure and/or Kjeldahl-N containing waste water being subjected to a nitrification in a first step and to denitrification in a subsequent step, in an aerated reactor which contains active sludge rich in nitrifying bacteria being used in the nitrification step and acid-neutralizing chemicals being added to said reactor if necessary and a high rate denitrification reactor which contains a very compact biomass which is capable of converting nitrate to nitrogen gas and to which an organic substrate is added being used in the denitrification step.

A method of this type is known from, inter alia, Agrarisch Dagblad of 14 March 1988. With this method the liquid fraction of fermented semi-liquid manure is treated. The biologically degradable organic substances, nitrifiable nitrogen and phosphorus which are present in the liquid fraction of anaerobic or fermented semi-liquid manure can be largely removed. The method essentially consists in a coupling of a nitrification step in a nitrification reactor in which ammonia is converted by bacteria to oxidized nitrogen with a denitrification step in a denitrification reactor in which oxidized nitrogen is converted by bacteria to nitrogen gas, the phosphate present in the liquid being concentrated as a chemical precipitate in the reactor at the same time. Oxidation of ammonia results in lowering of the pH, which with this method can be countered by metering in lime and/or metering in effluent from the denitrification reactor (recycling) to the nitrification reactor. During the nitrification step of this method there will also be some removal of nitrogen and phosphate by means of nitrogen and phosphate incorporation in the new cells of the active sludge. This nitrogen and phosphate was liberated during the fermentation of the manure whereby degradable substances yield CO_2 and CH_4 . With this method the nitrification reactor (which can be either a fed batch reactor or a batch reactor) is operated batchwise. It is then aerated until all ammonia has been nitrified, after which the aeration is stopped temporarily in order to allow the sludge to settle. The nitrified liquid manure is run off for treatment in the denitrification step, while the active sludge remains behind in the nitrification reactor for a subsequent cycle. In the denitrification step the effluent from the nitrification reactor is pumped upwards through a USB (upflow slub bed) reactor. In this reactor there is a very compact biomass which is capable of converting nitrate to nitrogen gas. In order to allow this step to proceed, an organic substrate - for example methanol - must be added to the reactor. Acid is consumed during the denitrification step, as a result of which the pH in the bacterial bed rises. As a consequence of this rise, an insoluble precipitate of phosphate with the calcium ions present in the liquid forms. The manure processing consisting of manure fermentation and separation of fermented manure, followed by the method for treatment of the liquid fraction of fermented semi-liquid manure, which has been described above, is shown in Figure 1. (The numerals of this and the following figures being explained in Table A).

A number of manure processing works are being developed at present, for example Promest in Helmond. In these works semi-liquid manure is evaporated to give a dry product, which costs a great deal of energy since semi-liquid manure consists of more than 90% of water. Moreover, this evaporation is a complex technology which in fact still has to be developed for use on manure. The cost price of processing of this type for the formation of dry granular or powder manure is consequently very high.

An approach which differs from that described above is the treatment of semi-liquid manure in conventional effluent treatment installations. Currently this is also being used for treatment of liquid manure from calves. The conventional manure treatment has the significant disadvantages that the process produces a large amount of sludge (excess bacteria) and that the process is not capable of removing the phosphate. This means that extra provisions have to be made for sludge treatment and dephosphating. A conventional manure treatment also requires a fairly large amount of space.

This method, as reported in Agrarisch Dagblad of 17 March 1988, has the advantage that it is relatively inexpensive and can be carried out in a compact installation. However, a number of problems also arise in this case in the treatment of fermented manure.

A compact manure treatment installation for manure and fermented manure or Kjeldahl-N containing waste water can be produced and maintained only if:

- a) the metering of the fermented liquid fraction is matched to the nitrification capacity of the nitrification reactor. The nitrification reactor must not be overloaded but must also not operate underloaded.
- b) The metering of methanol (or other sources of carbon) to the denitrification reactor is matched to the nitrate load in the denitrification reactor. In the case of undermetering not all nitrate is removed; in the case of overmetering, however, methanol (or other source of carbon) is present in the effluent to be discharged.
- c) The effluent recycling from denitrification reactor to nitrification reactor is controlled such that it is optimum. Too little recycling leads to a nitrate concentration which has an inhibitory action on the bacteria; too much recycling has the consequence that the reactor is filled mainly with liquid which has already been treated.

Said points can be achieved by the use of separate instruments, it being necessary to carry out some of

the diverse operations by hand. Moreover, the results of the various measurements cannot be integrated and translated into a control action without the intervention of one operator. Furthermore, the effluent from the nitrification reactor can still contain organic substances which cannot be further degraded in the nitrification reactor. Organic material which passes into the denitrification reactor can be converted into inorganic material in that reactor with the liberation of ammonium nitrogen which is then (insofar as it is not fed via the recycle stream) discharged with the effluent.

The aim of a copending European application 90.202728.3 is to eliminate these problems. It relates to a method of the type indicated in the preamble which is characterized in that the loading of the nitrification reactor is controlled and the optimum nitrification and denitrification are obtained on the basis of one or more of the following data:

- the incoming nitrogen load;
- the information from the WAZU respiration meter (Netherlands Patent Application No. 8600396, filed on 17 February 1986);
- the pH in the nitrification reactor, the criterion for which is that it is in the range limited by 6 and 8.5;
- the amount of air required
- the residence time
- the temperature in both the nitrification reactor and the denitrification reactor, the criterion for which is that this is lower than 40 °C;
- the concentration of oxidized nitrogen in the influent for the denitrification reactor, the criterion for which is that the concentration is between 0 and 4 g N/l;
- the concentration of oxidized nitrogen in the nitrification reactor, the criterion for which in the sludge/liquid mixture in the reactor is that the concentration is between 0 and 4 g N/l;
- the concentration of the carbon source in the effluent from the denitrification reactor;
- the gas production in the denitrification reactor.

An aspect of this process is that an instrument, a respiration meter (WAZU respiration meter), with which the time at which the treatment processes are complete is established and with which both Kjeldahl N concentration in the liquid fraction of fermented manure to be treated and the nitrate concentration of the effluent from the nitrification reactor (= feed for the denitrification reactor) can be calculated, can be used. However, it should be noticed that the use of such a respiration meter is not required. The other data mentioned are also sufficient for a good control of the process. The liquid streams and control lines in relation to the respiration meter are shown schematically in Figure 2. The respiration meter can control the entire method automatically on the basis of the data collated and calculated by the instrument. However, as already mentioned, such a respiration meter is certainly not necessary.

The nitrification is followed by a denitrification process.

Furthermore, the optimum conditions for the treatment methods have been investigated in both the nitrification and the denitrification reactor. The biomass in both the nitrification reactor and the denitrification reactor produce heat. Because of the high concentration of biomass and the high rates of conversion which are realized in both reactors, there will be a net excess of heat in both reactors if no measures are taken. It was found in laboratory experiments, that for a nitrifying bacterial population the optimum temperature of this bacterial population is between 31 and 35 °C and that the maximum temperature which can be tolerated is 40 °C. On the basis of general scientific information, it can be anticipated that the same temperature limits apply for the denitrifying bacterial population. Thermophilic denitrifying bacteria are known. These operate at temperatures above about 50 °C. However, for various reasons it is not desirable to use thermophilic organisms in the denitrification reactor: the effluent to be discharged will be much too warm and the recycle stream to the nitrification reactor may not be too warm. Both the nitrification and the denitrification reactor can be operated only if there is a provision for removal of heat from the respective reactor contents by a suitable means or due to cooling to the air by a suitable design.

For the present method, the conditions in the denitrification reactor must be kept such that phosphate can precipitate. The efficiency of the phosphate removal is dependent on the pH and the HCO_3/CO_2 ratio in the denitrification reactor.

The desired pH can be obtained by using an organic carbon source for the denitrification reactor with a specific chemical oxygen consumption (COC)/total organic carbon (TOC) ratio in the present method. The fact is that alkalinity (alkali, bicarbonate and carbonate) is produced in the denitrification reactor under the influence of the denitrification reaction. The production of alkalinity is dependent on the COC/TOC ratio of the organic C source in the denitrification reaction. Usually methanol is used as organic C source. Methanol has a high COC/TOC ratio and results in a higher production of alkalinity than, for example, glucose, which has a much lower COC/TOC ratio. Experiments have shown that the COC/TOC ratio must be 3.75 or below.

As stated, the pH falls in the nitrification reactor on the oxidation of the ammonia. To counter

acidification of the reactor, an alkali can be metered in or effluent can be recycled from the denitrification reactor to the nitrification reactor. It has been established experimentally that the concentration of oxidized nitrogen in the nitrification reactor in the sludge/liquid mixture is between 0 and 4 g N/l and preferably is in the range limited by 0 and 1.5 g N/l. Furthermore, it has been found that the concentration of oxidized oxygen in the influent for the denitrification reactor is between 0 and 4 g N/l and is preferably between 1.0 and 1.4 g N/l. In order to achieve this, the effluent from the denitrification reactor can be recycled. This recycling provides dilution of the concentration of oxidized nitrogen at the feed location in the reactor. Furthermore, this recycling is intended to obtain a higher stream velocity in the denitrification reactor, which promotes the contact between biomass and substrate in the reactor. Recycling can take place directly from effluent stream to influent stream for the denitrification reactor. It is, however, also possible (and in fact better for the overall process) for recycling of effluent from the denitrification reactor to be used, this recycling taking place entirely or partially via the nitrification reactor. The aim of this is then to achieve both a saving in the chemicals consumption for pH control in the nitrification reactor and to achieve a dilution of the reactor contents of the nitrification reactor such that the content of oxidized nitrogen is always lower than 4 g N/l.

An other aspect is the use of a separation step, e.g. a physical/chemical flocculation step and a floccule separator or a membrane technology after the nitrification step. Purpose of said separation previous to the denitrification reactor is catching suspended and colloiddally dissolved organic substances, that otherwise would mineralize in the denitrification reactor resulting in the formation of ammonia nitrogen. A physical/chemical flocculation step plus floccule separation is shown schematically in Figure 3. The residual organic substance can be removed from the effluent with the aid of flocculating adjuvants and a process for separation of the flocculant from the effluent. By positioning upstream of the denitrification step, the organic substances can be removed before they are converted to inorganic substances and ammonium nitrogen is formed. A further advantage of this is that the carbonate content in the effluent from the nitrification reactor is low (lower than in the effluent from the denitrification) reactor, to which organic substrate is added). This is advantageous if a flocculating adjuvant is used which forms a precipitate with carbonate. If a flocculating adjuvant is used which contains cations which precipitate with phosphate, an additional phosphate removal is performed.

The copending application also relates to an installation which is suitable for carrying out the method as described above, comprising:

- a nitrification reactor which is provided with aeration, feed of liquid to be treated, feed of acid-neutralizing chemicals, active sludge rich in nitrifying bacteria, sludge discharge, effluent discharge;
- a line through which the effluent from the reactor can be fed to the denitrification reactor;
- a denitrification reactor which is provided with feed of effluent from the nitrification reactor, feed of a carbon source, an upflow slub bed (USB) column, a very compact biomass capable of converting nitrate to nitrogen gas, phosphate-rich sludge discharge, effluent discharge, nitrogen gas discharge;
- a line through which the effluent from the denitrification reactor can be discharged.

In the most simple form, the installation (shown schematically in Figure 2) consists of the combination of a batch reactor (to which all influent (7) is added at once per cycle) or a fed batch reactor (to which the influent is added gradually or stepwise per cycle) as nitrification reactor (9) and a continuously fed upflow slub bed (USB) reactor as denitrification reactor (13). The two reactors are operated connected in series, without bypass of the nitrification reactor (9) but optionally with backmixing (33) from the denitrification reactor (13) to the nitrification reactor (9).

The use of the WAZU respiration meter (18) (Netherlands Patent Application 86.00396, filed on 6 February 1986), a measurement and control unit with which the course of the respiration rate of the biomass in the reactor (9) is followed, is characteristic of the installation according to the copending application.

The nitrification reactor (9) of the apparatus is provided with aeration (10), a feed of liquid (7) to be treated, a sludge discharge (11) and optionally a feed of effluent from the denitrification reactor (33), all of which are controlled by the WAZU respiration meter (18) (Netherlands Patent Application 86.00396, filed on 6 February 1986). This respiration meter also controls the metering of the source of carbon (14) for the denitrification reactor (13). This denitrification reactor is additionally provided with nitrogen gas discharge (17) and effluent recirculation (33) or discharge (16).

Another embodiment of the installation according to the copending application (shown schematically in Figure 4) is also provided with a line (32) through which the effluent from the denitrification reactor (13) can be partially recycled to the influent (12) for the denitrification reactor (13) and additionally this installation is provided with a feed of one or more acid-neutralizing chemicals (8) to the nitrification reactor (9).

Furthermore, the apparatus can comprise a combination of the two above installations (Figures 4 and 5), i.e. an installation as shown in Figure 6, this installation being provided with a line through which the

effluent (32, 33) from the denitrification reactor (13) can be partially recycled (33 and 32 respectively) to the nitrification reactor (9) and to the influent (12) for the denitrification reactor (13).

The three lastmentioned installations, shown in Figures 4, 5 and 6, can comprise a further addition (see Figure 7) in the form of a feed of chemicals for phosphate precipitation (20).

Furthermore, all of these installations (shown in Figures 4, 5, 6 and 7) can be provided with one or more flocculation installations (19). The flocculation installation as such is shown schematically in Figure 3.

The apparatus according to the copending application which have already been described can be provided with the flocculation installations at various locations (Figures 8, 9 and 10). In the installation according to Figure 8, the flocculation installation (19) is positioned in such a way that the effluent (16) from the denitrification reactor (13) flows through the flocculation installation (19 and Figure 3) upstream of the recycle (34, 35) or discharge (16).

In the installation according to Figure 9, the flocculation installation (19) is positioned in such a way that only the effluent (16) from the denitrification reactor (13) which is to be discharged flows through the flocculation installation (19).

In the installation according to Figure 10, which is preferred, the flocculation installation (19) is positioned in such a way that the effluent (12) originating from the nitrification reactor (9) flows through the flocculation installation (19) before it flows into the denitrification reactor (13).

The apparatus according to the copending application in which the nitrification reactor is provided with feed of the effluent (16, 33, 34) from the denitrification reactor (13) can be provided with a spray installation (25 in Figure 10) through which the effluent (16, 33, 34) from the denitrification reactor (13) can be sprayed into the nitrification reactor (9) to prevent foam formation.

Furthermore, all installations according to the copending application can be provided with one or more buffer tanks (23) (Figure 10).

In the above process, all effluent from the nitrification reactor passes through the separator, this means a high load for the separator.

It has now been found that an improvement can be reached by partially recirculating the effluent from the nitrification reactor (9) to the denitrification reactor (13), adding a source of carbon to the effluent to be passed to the denitrification reactor (13) and passing part of the effluent stream from the nitrification reactor (9) to a separation unit to separate sludge, the effluent from the separation step (5) is passed to an other denitrification reactor (37) (see fig. 11). When necessary a source a carbon can be added to the nitrification reactor. The effluent from the denitrification reactor (37) can be discarded. The scheme of the apparatus is shown in fig. 11.

Surprisingly it has been found, that the sludge present in the effluent recirculated to the denitrification reactor (13) and subsequently recirculated to the nitrification reactor (9) has no disadvantageous effect on the process.

The process is especially suited for processing manure (that can be fermented) or Kjeihdahl-N containing waste water.

The above process can be improved by using two different types of denitrification reactors; the effluent denitrification reactor (37) and the recirculation denitrification reactor (13). The effluent from the nitrification reactor (9) is partially recirculated from the nitrification reactor to the recirculation denitrification reactor (B). An organic carbon source can be added to the influent of this denitrification reactor in order to provide sufficient organic carbon substrate for the denitrification reaction.

In the lay-out of the apparatus of the invention it is no longer detrimental when the effluent of the denitrification reactor (13) still contains a small amount of nitrate. This because the effluent from this reactor is passed to the nitrification reactor (9). The metering of the organic carbon source is in this reactor less critical then in the process of the copending application. The other part of the effluent of the nitrification reactor is passed to the effluent denitrification reactor (37).

An organic carbon source can also be supplied to the influent of the denitrification reactor (37). Of course it is not advisable to use here part of the influent to be treated according to the process of the invention. This because the effluent of this denitrification reactor is to be discarded. This embodiment using part of the influent of the system can only be used in denitrification reactor (13). The apparatus can further comprise a pipe flocculator (38). The reaction scheme is shown in fig.12. As already has been elucidated above, a separation step can be used for the removal of phosphorus and suspended and colloiddally dissolved organic substances. In the process of the invention with a recirculation denitrification reactor (13) and an effluent denitrification reactor (37) the separation step (5) can be positioned in the influent stream of the effluent denitrification reactor (37). The hydraulic load of the separation step is than much lower than in the copending application. This is shown in fig. 13. However, when the separation step is placed downstream the effluent denitrification reactor still some ammonium and biodegradable soluble organic

substances are formed from organic material in the denitrification reactor (13). These soluble organic biodegradable substances and ammonium will pass unchanged through the separation step (5) and will be discarded. By placing the separation step upstream the effluent denitrification reactor the organic matter will be removed before passing through the effluent denitrification reactor, so that no ammonium or soluble organic substances will be formed here.

This is shown in figure 14.

By using two different types of denitrification reactors it is also possible to add the feed at the influent of the recirculation denitrification reactor (13). By doing this it is possible to use the organic material which is in the feed as a carbon source for the denitrification process. The ammonium in the feed will pass unchanged through the recirculation denitrification reactor (13) and will be added by the recirculation stream at the nitrification reactor (9). Here the ammonium will be oxidized to nitrate. Most of the oxidizable organic matter in the feed stream will be used for denitrification. If there is still some oxidizable organic matter left in the effluent stream of the recirculation denitrification reactor (13) this organic matter will be oxidized in the nitrification reactor (9).

The effluent of the nitrification reactor (9) will partially be put through the recirculation denitrification reactor (13). To this effluent for the recirculation denitrification reactor (13) the feed with organic matter and ammonium will be added, so that the nitrate in this part of the effluent from the nitrification reactor (9) will be denitrified here. The other part of the effluent of the nitrification reactor (9) passes through the separation step (5), if this is necessary in view of pollution exigences. A carbon source is added to the effluent of the separation step (e.g. methanol). This stream is then put through the effluent denitrification reactor (37), where the nitrate is converted into nitrogen gas. The effluent of this reactor is then discarded. This is shown in drawing 15.

By adding the feed at the influent of the recirculation reactor (13) the recirculation ratio (= amount of influent for the recirculation denitrification reactor (13) without feed divided by the amount of feed) is determined by several points:

- the nitrate concentration in the nitrification reactor should be less than 1.5 g N/l;
- the amount of alkalinity in the effluent of the recirculation denitrification reactor (13) should be enough to counter acidification in the nitrification reactor (9);
- the use of an external carbon source (e.g. methanol) should be limited;
- the hydraulic loading of the nitrification reactor (9) and the recirculation denitrification reactor (13) should not be too big.

To meet these points it can be necessary to add a part of the feed at the nitrification reactor (9) and another part to the influent of the recirculation denitrification reactor (13). In this case it can be necessary to add also an external carbon source as methanol to the recirculation denitrification reactor (13) (Shown schematically in drawing 16). This process can be operated with or without a separation step.

Furthermore, the process can be provided with one or more buffer tanks. The buffer tank (3) in which the effluent from the nitrification reactor is collected can be constructed like a sedimentation tank, so that surplus sludge from the nitrification reactor (9) can settle here and can be removed. The effluent from this buffer tank is partially passed through the recirculation denitrification reactor (13) and partially passed through the separation step (5).

The effluent from the recirculation denitrification reactor (13) can be collected in a buffer tank (9). This buffer tank can also be constructed like a sedimentation tank, so that sludge still present in the effluent of the recirculation denitrification reactor can settle here. This sludge can be returned to the reactor, or can be removed as surplus sludge. The effluent from this buffer tank is put in the nitrification reactor.

The effluent of the effluent denitrification reactor can also be collected in a sedimentation tank. The sludge still present in the effluent of the effluent denitrification reactor can settle here and returned to the denitrification reactor or can be removed as surplus sludge. The effluent from this sedimentation tank will be discharged. This is schematically shown in drawing 17.

It will be clear that this different lay out of the installation can be used with all the embodiments described above. According to a beneficial embodiment an amount of influent can be used as a carbon source.

According to the present invention the separation unit (5) can use the conventional separation methods such as centrifugation, sedimentation and so forth, however, also the use of membrane technology is possible. In this case the filtration is applied followed by a phosphate removal by precipitation.

An other possibility to remove organic material is chemical oxidation using ozon or hydrogen peroxyde, for instance.

The invention is illustrated by means of the following example that only serves for illustrative purposes and is not limiting for the scope of the invention.

Example

Fermented manure (i.e. the liquid fraction obtained by centrifugation of anaerobic fermented liquid pig manure) is treated in the apparatus of fig. 11.

5 Analysis of the fermented manure shows a COD concentration of 21000 mg/l, a nitrogen concentration of 6500 mg N/l and a phosphorus concentration of 275 mg P/l.

The apparatus shown in fig. 11 consists of a nitrification reactor (9) having a usable volume of 50 m³, two recirculation denitrification reactors (13 and 37) which are positioned parallel to each other each having a usable sludge bed volume of 10 m³, a separator consisting of a pipe flocculator (38) and a centrifuge (5) 10 and one effluent denitrification reactor (37) having usable sludge bed volume of 5 m³.

The nitrification reactor in this example is a fed batch reactor with a stepwise addition (0,5 m³ of manure per step) of fermented manure. A total of 2 m³ is added in four steps.

In the total cyclus of the nitrification reactor 8 m³ of effluent of the denitrification reactor is supplied by sprayers proportionally distributed in time. After a total of 2 m³ fermented manure has been introduced in 15 the nitrification reactor and all ammonium nitrogen has been nitrified the aeration is ended and active sludge is allowed to sediment during sixty minutes. After the sedimentation period 10 m³ of the supernatant liquid is discharged as an effluent of the nitrification reactor. Then a new cyclus is started wherein again 2 m³ of fermented manure and 8 m³ of effluent of the denitrification are added.

A WAZU respiration meter (trade mark RA-1000 marketed by Manotherm) is coupled to the nitrification 20 reactor to monitor the actual respiration velocity. Further the oxygen concentration in the nitrification reactor is monitored with an oxygen sensor.

The blower which is used for the supply of oxygen by means of air is controlled by the oxygen concentration in the nitrification reactor. The oxygen concentration is kept at 2.0 mg/l.

After addition of 0.5 m³ of fermented manure the actual respiration velocity increases and the blower 25 velocity increases also to keep the oxygen concentration at 2.0 mg/l. When the ammonium added with the fermented manure is nitrified the actual respiration velocity decreases to the basis level and the blower velocity has to decrease as well. After falling underneath the setpoint for the respiration velocity and/or the setpoint for the blower velocity another 0.5 m³ of fermented manure is added to the nitrification reactor. Figure 18 gives the oxygen concentration and the blower velocity as a function of time. The average dose 30 of the fermented manure in the present nitrification reactor was in this test about 6 m³ a day.

The pH value is also measured in the nitrification. Lime milk is supplied when the pH-value is below 6.5. The temperature is also monitored and is kept at a value below 33 °C by means of a heat exchanger.

The effluent of the nitrification reactor has a nitrate-N concentration of 1100 mg N/l and a phosphate-P concentration of 125 mg P/l. The nitrate-N concentration is lower than could be expected on the basis of the 35 dilution of the reactor contents with effluent from the denitrification reactor. This is the consequence of some denitrification in the nitrification reactor during the sedimentation period and the incorporation of nitrogen in the biomass.

The effluent of the nitrification reactor is collected in a buffertank (3). This tank is constructed like a sedimentation tank, so that sludge what is still present in the effluent of the nitrification reactor, can sediment 40 here.

Four-fifth of the contents of the buffertank is put through two recirculation denitrification reactors that have been arranged parallel. Methanol is added on the basis of the nitrate-N-concentration in the influent stream. The methanol dose is about 1.65 kg/m³ influent of the denitrification reactor. The denitrification 45 proces is monitored by means of the gasproduction (1630 l/h). The pH-value of the denitrification reactors is between 9.0 and 9.3. The temperature is kept below 35 °C by means of a heat exchanger.

The effluent of these two denitrification reactors is collected in a buffertank (23). From this buffertank the effluent is pumped through sprayers, which are situated on the top of nitrification reactor, in the nitrification reactor.

One fifth of the effluent from the nitrification reactor is pumped through a pipe flocculator. At the 50 beginning of this flocculator a 38 w% (weight/weight) solution of FeCl₃ (iron(III)chloride) is dosed in an amount of 10 l/m³ effluent of the nitrification reactor (9). In the middle of the pipe flocculator lime milk or caustic soda is supplied until the pH-value is 5.5. At the end of the pipe flocculator polyelectrolyte is dosed (180 mg per m³ effluent of the nitrification reactor). The liquid then passes through a centrifuge separating in a liquid stream and a sludge stream. The sludge production is about 0.36 m³/d. The nitrate-N 55 concentration and phosphate-P concentration in the effluent of the centrifuge amount 1100 mg N/l and < 0.5 mg P/l respectively.

The effluent of the centrifuge (5) is then put through the effluent denitrification reactor (37). Methanol is added on basis of the nitrate-N concentration in the influent stream. The denitrification proces is monitored

by means of the gasproduction (408 l/h). The pH value is below 9.0. Temperature is kept below 35°C by means of a heat exchanger.

The effluent of the denitrification is put through a sedimentation tank and is discharged.

5

Table A

Explanation of the numerals in the figures

- | | |
|----|---|
| 10 | 1. Storage of semi-liquid manure |
| | 2. Fermentation installation |
| | 3. Biogas |
| | 4. Installation for energy generation |
| 15 | 5. Installation for separation |
| | 6. Cake |
| | 7. Filtrate = liquid fraction to be treated |
| 20 | 8. Holder for metering acid-neutralizing chemicals |
| | 9. Nitrification reactor |
| | 10. Air supply |
| | 11. Sludge discharge |
| 25 | 12. Effluent from the nitrification reactor |
| | 13. Denitrification reactor |
| | 14. Holder for metering C source |
| | 15. Phosphate-rich sludge |
| 30 | 16. Effluent from the denitrification reactor |
| | 17. Nitrogen gas |
| | 18. WAZU respiration meter |
| 35 | 19. Separation installation |
| | 20. Holder for chemicals for phosphate precipitation |
| | 21. Sludge, flocculated material |
| 40 | 22. Effluent originating from the flocculation installation, positioned downstream of the denitrification reactor |
| | 23. Buffer tank |
| | 24. Storage of discharged sludge |
| | 25. Spray installation |
| 45 | 26. Influent pump |
| | 27. Static mixer and/or flocculating tank |
| | 28. Centrifuge |
| 50 | 29. Sludge pump |
| | 30. Iron chloride storage |
| | 31. Metering pump |
| 55 | 32. Effluent originating from the denitrification re-actor which recycles to the denitrification reactor |

33. Effluent originating from the denitrification reactor which recycles to the nitrification reactor
- 5 34. Effluent originating from the separation step, which is positioned downstream of the denitrification reactor, which flows to the nitrification reactor
- 10 35. Effluent originating from the separation step, which is positioned downstream of the denitrification reactor, which recycles to the nitrification reactor
- 15 36. Effluent originating from the separation step, which is positioned upstream of the denitrification reactor.
37. Denitrification reactor
38. Pipe flocculator
- 20 39. Effluent discharge

Claims

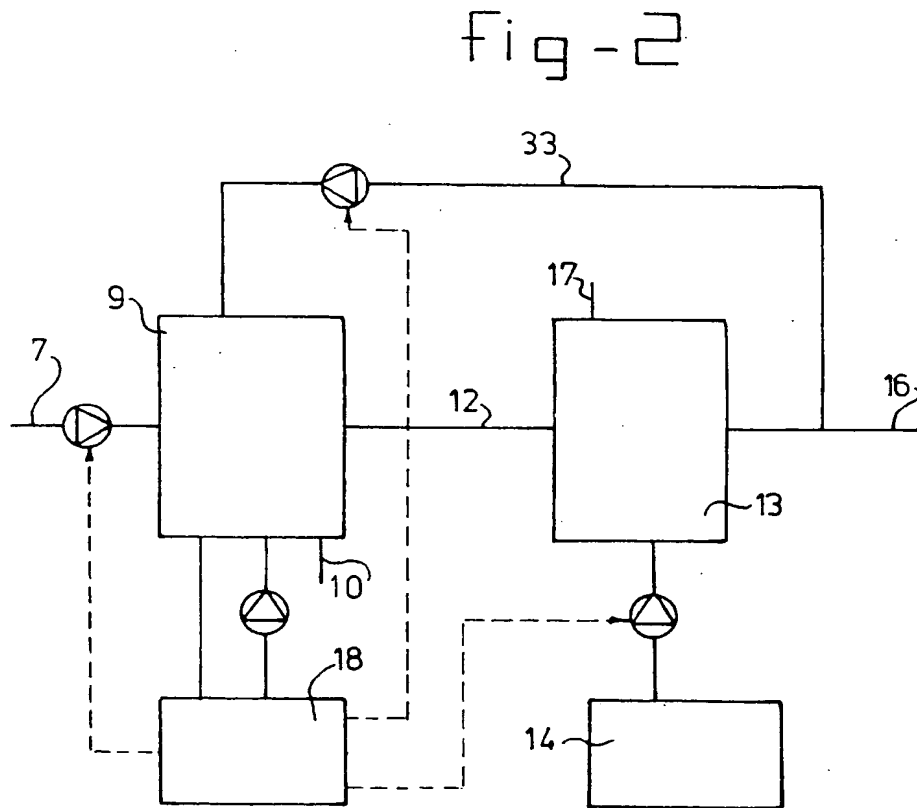
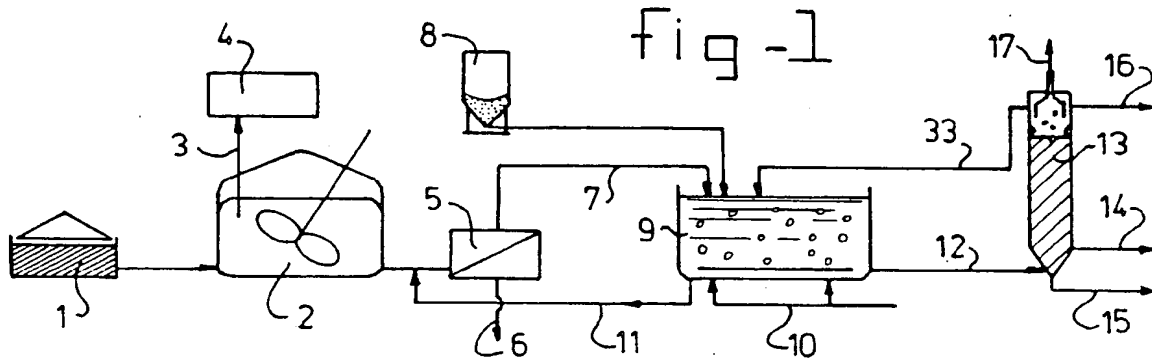
- 25 1. Method for processing manure, liquid manure and/or Kjeldahl-N containing waste water being subjected to a nitrification in an aerated reactor (9) which contains active sludge rich in nitrifying bacteria being used in the nitrification step and acid-neutralizing chemicals being added to said reactor (9) if necessary and to a denitrification in a high rate denitrification reactor (13) which contains a very compact biomass which is capable of converting nitrate to nitrogen gas and to which an organic substrate is supplied obtained from the denitrification step in reactor (9), characterized in that the loading of the reactor (9) is controlled to obtain an optimum nitrification and denitrification and this is obtained on the basis of one or more of the following data:
- 30
- the incoming nitrogen load;
 - 35 - the information from a WAZU respiration meter (not shown);
 - the oxygen concentration in the nitrification reactor (9)
 - the pH value in the nitrification reactor (9), the criterion for which is that the pH value is in the range limited by 6 and 8.5;
 - the amount of air required
 - 40 - the residence time
 - the temperature in both the nitrification reactor (9) and the denitrification reactor (13) is kept below 40 °C;
 - the concentration of oxidized nitrogen in the influent for the denitrification reactor (13), the criterion for which is that the concentration is between 0 and 4 g N/l;
 - 45 - the concentration of oxidized nitrogen in the nitrification reactor (1), the criterion for which in the sludge/liquid mixture in the reactor is that the concentration is between 0 and 4 g N/l;
 - the concentration of the carbon source in the effluent from the denitrification reactor (13);
 - the gas production in the denitrification reactor (13)
 - the effluent from the nitrification reactor (9) partially being passed to the denitrification reactor (13), adding a source of carbon to the effluent to be passed to the denitrification reactor (13) and passing an other portion of the effluent stream from the nitrification reactor (9) to a separation step (5) to separate a sludge (18) the effluent from separation step (5) being passed to a denitrification reactor (37) under the addition of a carbon source if desired, the denitrification reactor (37) being provided with an effluent discharge (38) and a nitrogen discharge (21).

50
- 55 2. The method according to claim 1, characterized in that the effluent from the nitrification reactor (1) is (first) passed through a buffer tank (3), provided (with a means to remove sludge and with) a discharge (4) to separation step (5) and a discharge (9) to denitrification reactor (2) buffer tank (3) further being

provided with a discharge (19) to denitrification reactor (6).

3. The method according to claim 1 or 2, characterized in that liquid from the denitrification reactor (2) is recycled to the nitrification reactor (1).
- 5 4. The method according to claim 2 or 3, characterized in that the effluent stream from the nitrification reactor (1) passed to the separation step (5) is subjected to a physical chemical treatment.
- 10 5. The method according to claim 4 characterized by the addition of a flocculating substance containing cations which can precipitate with phosphate, such as, for example, iron chloride.
6. The method according to claim 5, characterized in that iron chloride is used.
- 15 7. The method according to claim 2 to 6, characterized in that the recycled liquid is passed to the nitrification reactor 2 and or 6 via a spray installation.
8. The method according to claim 2 to 7, characterized in that part of the effluent is also recycled to the influent of the denitrification reactor (13).
- 20 9. The method according to one of the preceding claims, characterized in that the nitrification reactor (1) used is a batch reactor or a fed batch reactor (with a continuous or batchwise addition of influent).
10. The method according to one of the preceding claims, characterized in that chemicals for phosphate precipitation are added to the denitrification reactor (6).
- 25 11. The method according to claim 10, characterized in that Ca^{+2} , Fe^{+2} , Fe^{+3} , Mg^{+2} and/or Al^{+3} are used.
12. The method according to one of the claims 1-10, characterized in that methanol is added as an organic substrate to the denitrification reactor (2) and/or (6).
- 30 13. The method according to one of the claims 1-11, characterized in that glycol is added as organic substrate to the denitrification reactor (2) and/or (6).
- 35 14. The method according to one of claims 1-13, with which an organic substance or a mixture of organic substances is added to the denitrification reactor (2) and/or (6), characterized in that a ratio between chemical oxygen consumption and total organic carbon (COC/TOC ratio) of less than or equal to 3.75 is maintained.
- 40 15. The method according to one of claims 1 to 14, characterized in that the influent to be treated is fully or partially supplied to reactor (2).
16. The method according to one of the preceding claims, characterized in that one or more acid-neutralizing chemicals are added to the nitrification reactor (1).
- 45 17. The method according to claim 16, characterized in that lime is added.
18. The method according to one of claims 1-15, characterized in that the pH value in the nitrification reactor is maintained at 7-8.
- 50 19. The method according to one of the preceding claims, characterized in that the temperature in both the nitrification reactor (1) and in the denitrification reactor (5) is maintained at 20-35° Celsius.
- 55 20. The method according to one of claims 1 to 19, characterized in that the concentration of oxidized nitrogen in the influent for the denitrification reactor is maintained at 1.0-1,4 g N/l.
21. The method according to one of the claims 1 to 20, characterized in that the concentration of oxidized nitrogen in the nitrification reactor is maintained at 0-1.5 g N/l.

22. An apparatus suitable for carrying out the method according to one of the preceding claims, comprising:
- a nitrification reactor (1) which is provided with an aeration (10); feed of liquid (11) to be treated, with a feed of acid-neutralizing chemicals (12), active sludge rich in nitrifying bacteria (13), a sludge discharge (14), an effluent discharge (15);
 - a line (9) through which part of the effluent (15) from the nitrification reactor (1) can be fed to the denitrification reactor (2);
 - a denitrification reactor (2) which is provided with a feed of effluent (16) from the nitrification reactor (1), a feed of a carbon source (17), a discharge (18), effluent discharge (17) to reactor (1); characterized in that the installation (shown schematically in figure 2) is constructed such that part of the effluent from reactor (1) is passed to denitrification reactor (2) and part is passed to separation unit (5) provided with a sludge discharge (18) and an effluent discharge (19) connected with a denitrification reactor (6) with an effluent discharge (20) and a nitrogen outlet (21).
23. Apparatus according to claim 22, characterized in that it is provided with a feed of chemicals for phosphate precipitation (22).
24. Apparatus according to claims 22 or 23, characterized in that this is provided with buffer tanks (22 and 7 in drawing 2).
25. Apparatus according to claims 22 to 24, characterized in that it is provided with a means for chemical phosphate precipitation (not shown) are ranged between (5) and (6).
26. Apparatus according to claims 22 to 25, characterized in that it is provided with means to catch sludge after (3), (2) and/or (6).
27. Apparatus according to claims 22 to 26, characterized in that buffer tanks (3) and (7) are provided with means to remove sludge.
28. Apparatus according to claims 21 to 27, characterized in that discharge (20) is provided with means to remove sludge.
29. Apparatus according to claims 22 to 28, characterized in that it is provided with means to recirculate sludge from (3) to (1), from (7) to (2) and/or from (6) to (6).



---- CONTROL LINES
 ——— LIQUID LINES
 - - - - - OPTIONAL LIQUID LINES

fig - 3

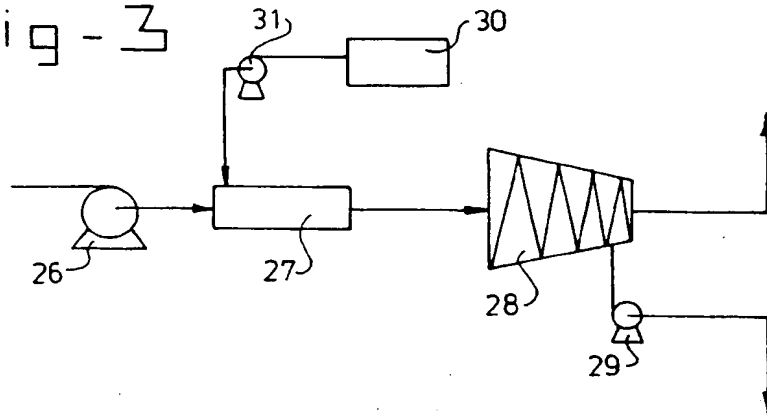


fig - 4

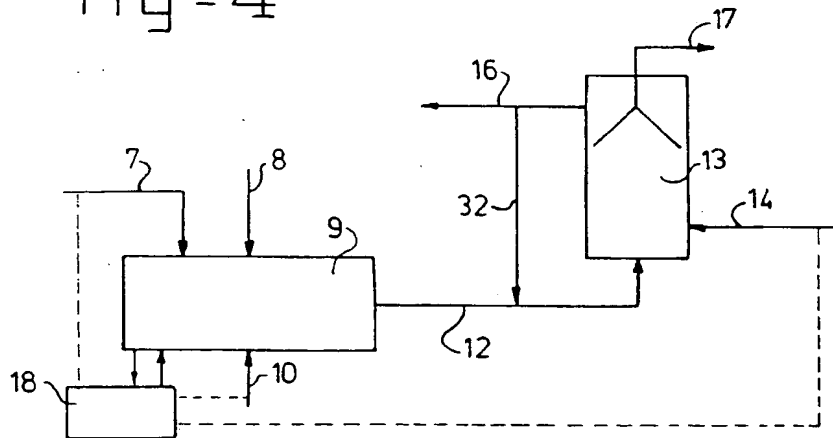


fig - 5

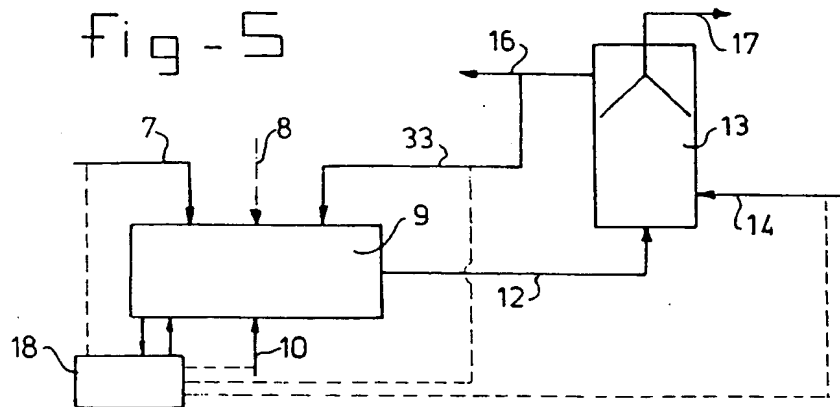


fig - 6

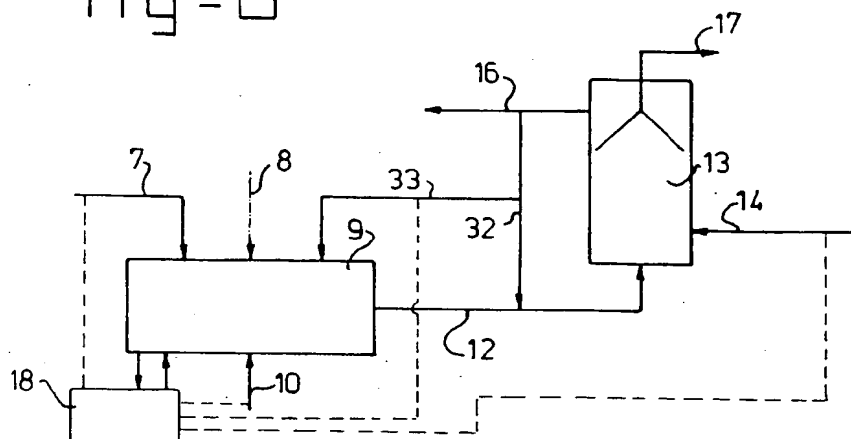


fig - 7

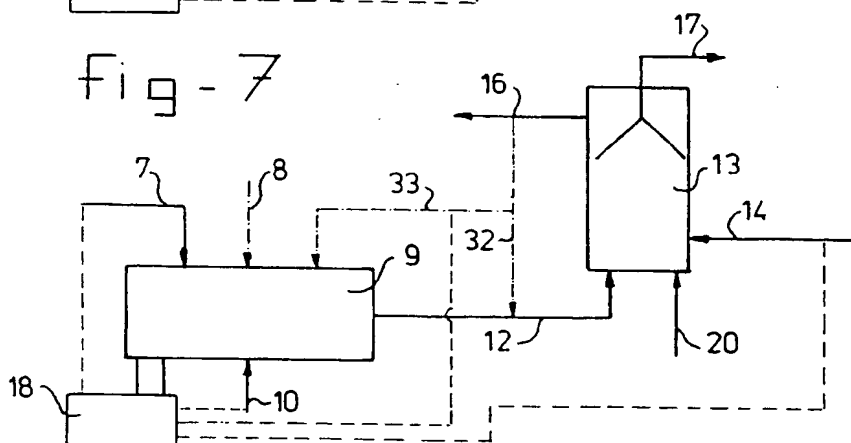
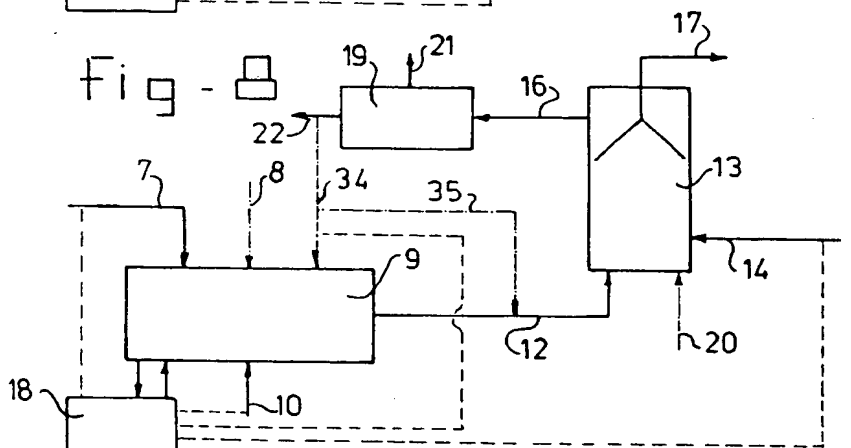


fig - 8



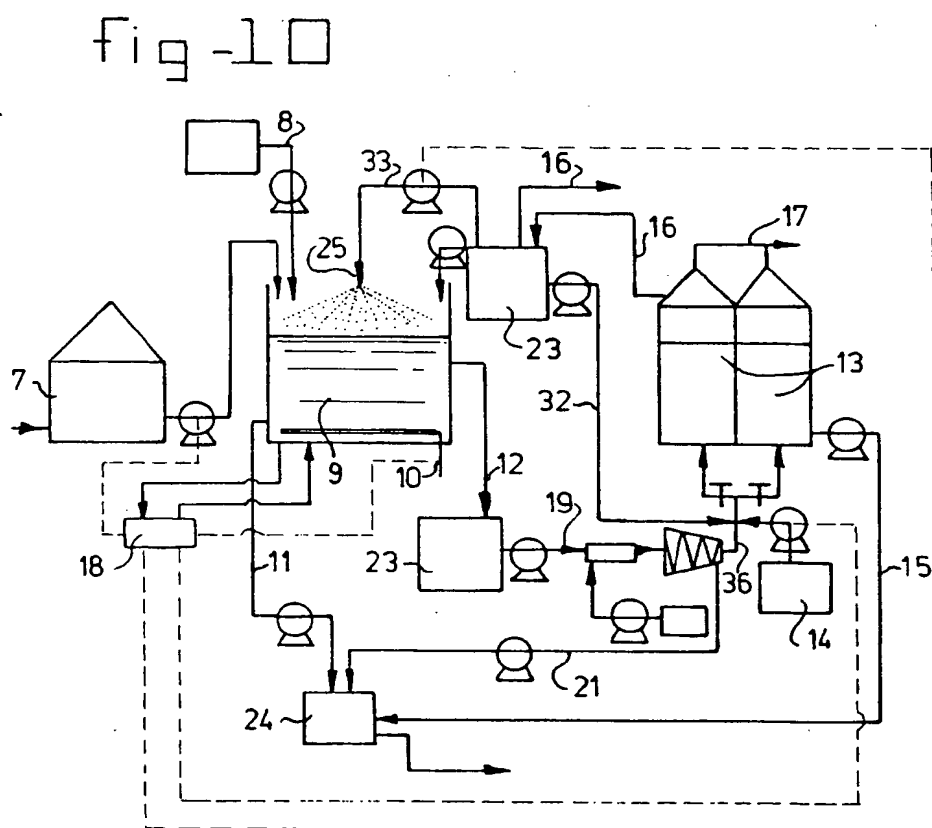
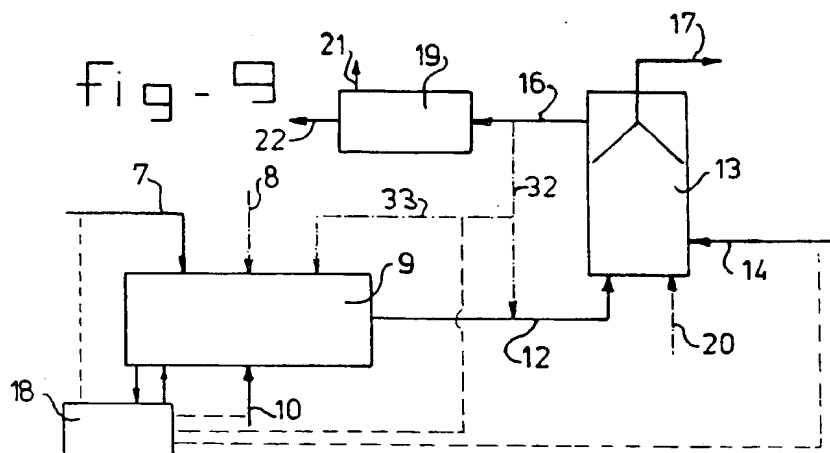


fig - 11

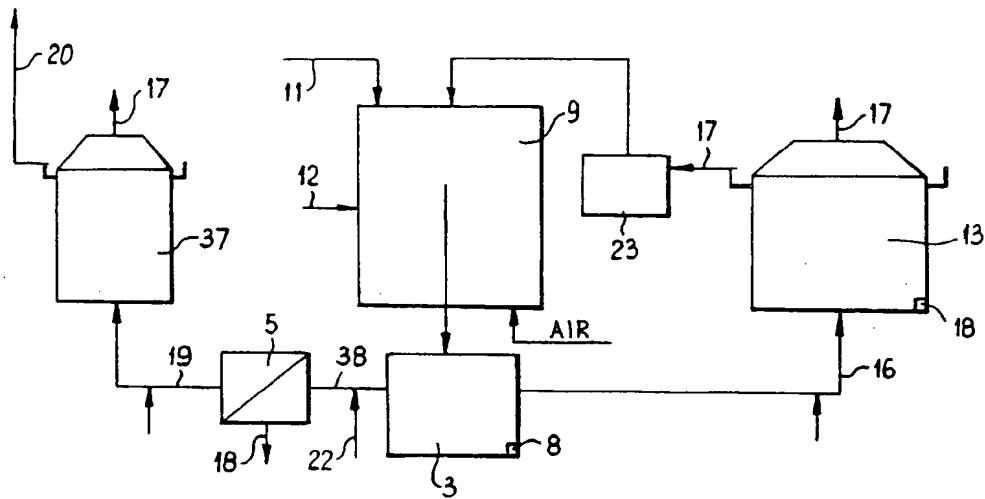


fig - 12

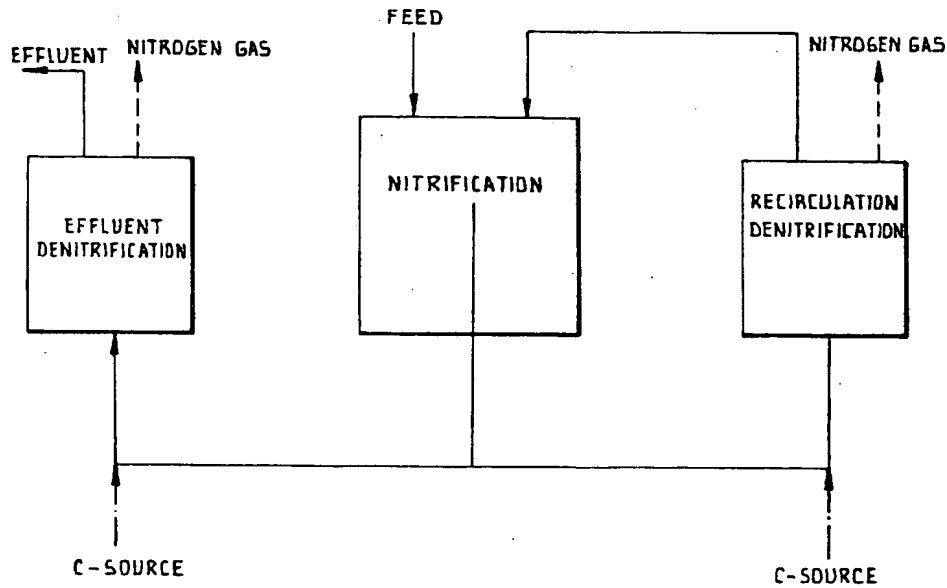


fig - 13

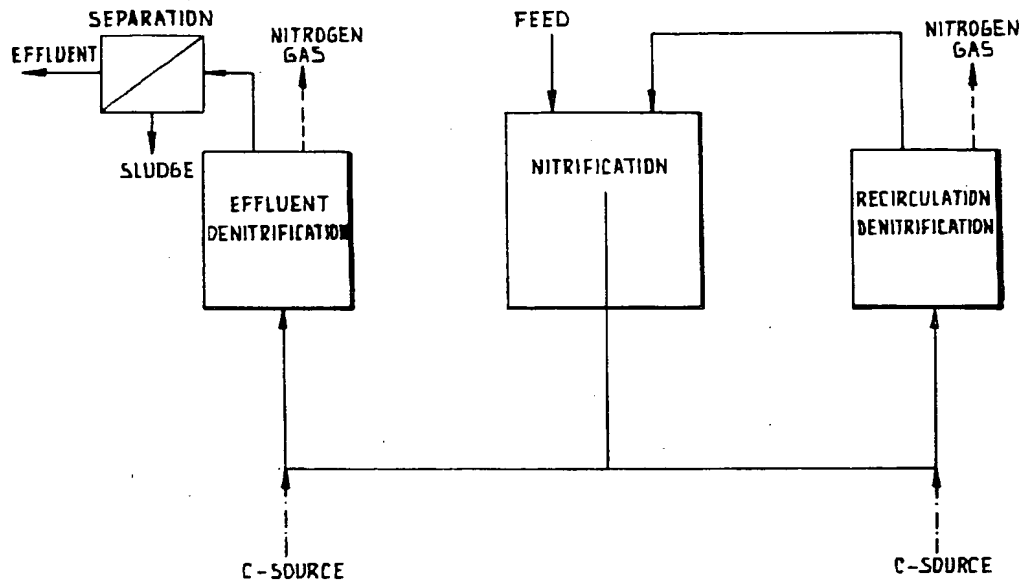


fig - 14

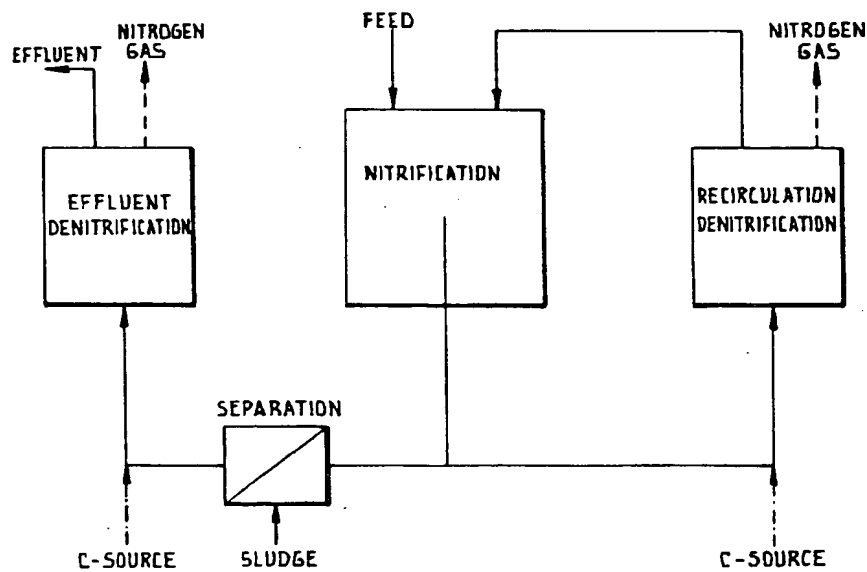


fig - 15

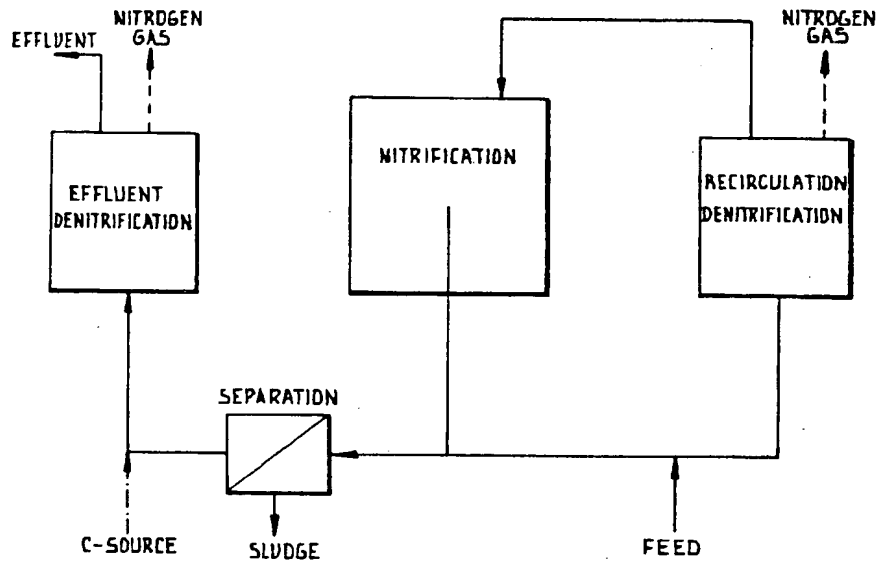


fig - 16

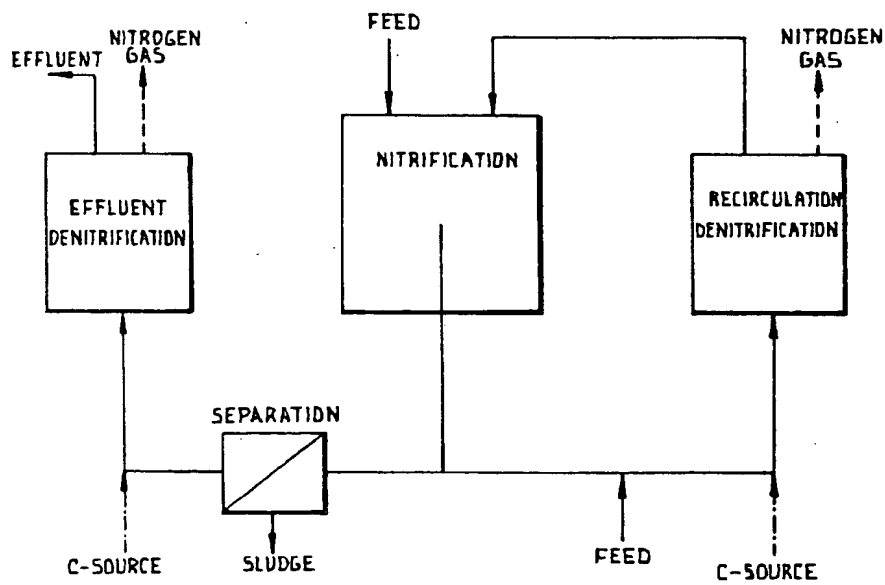


fig-17

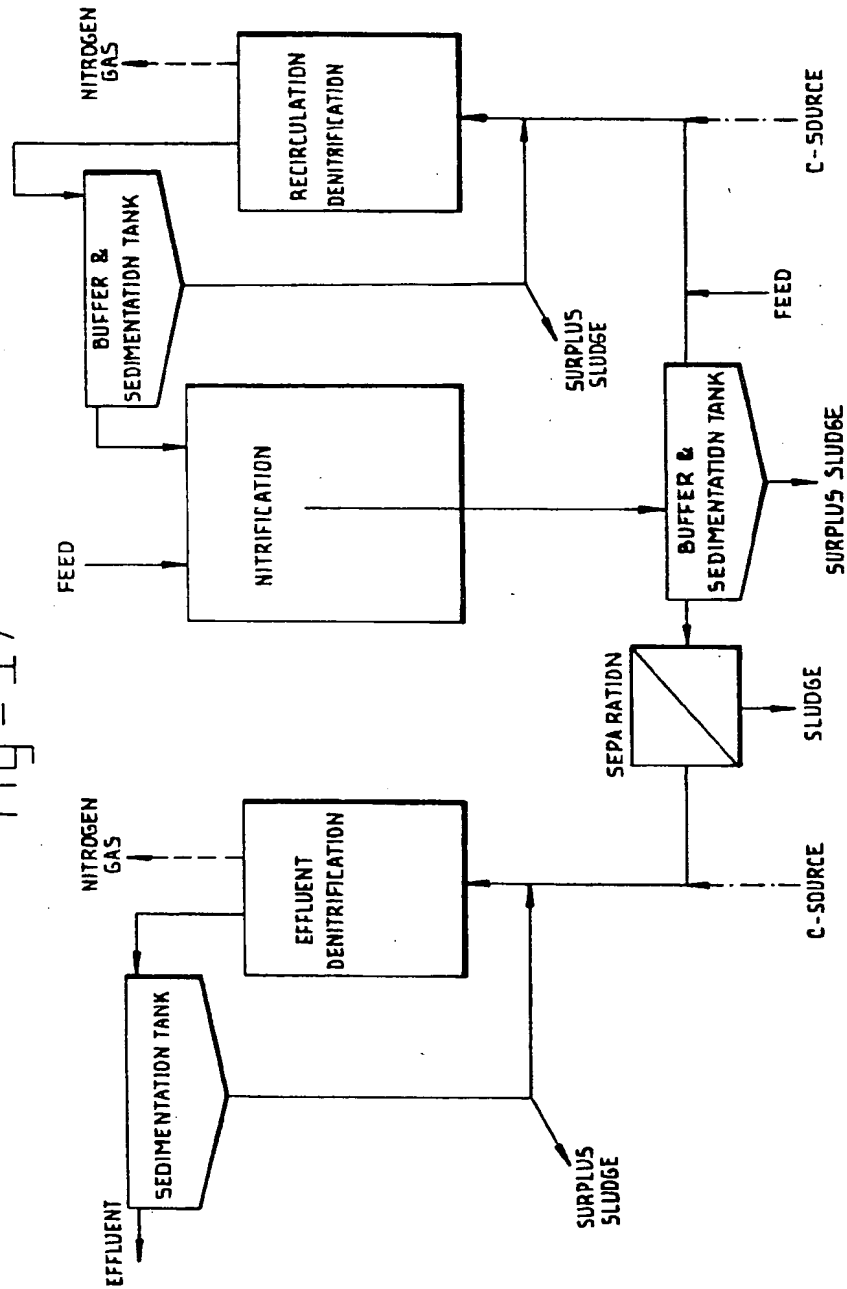
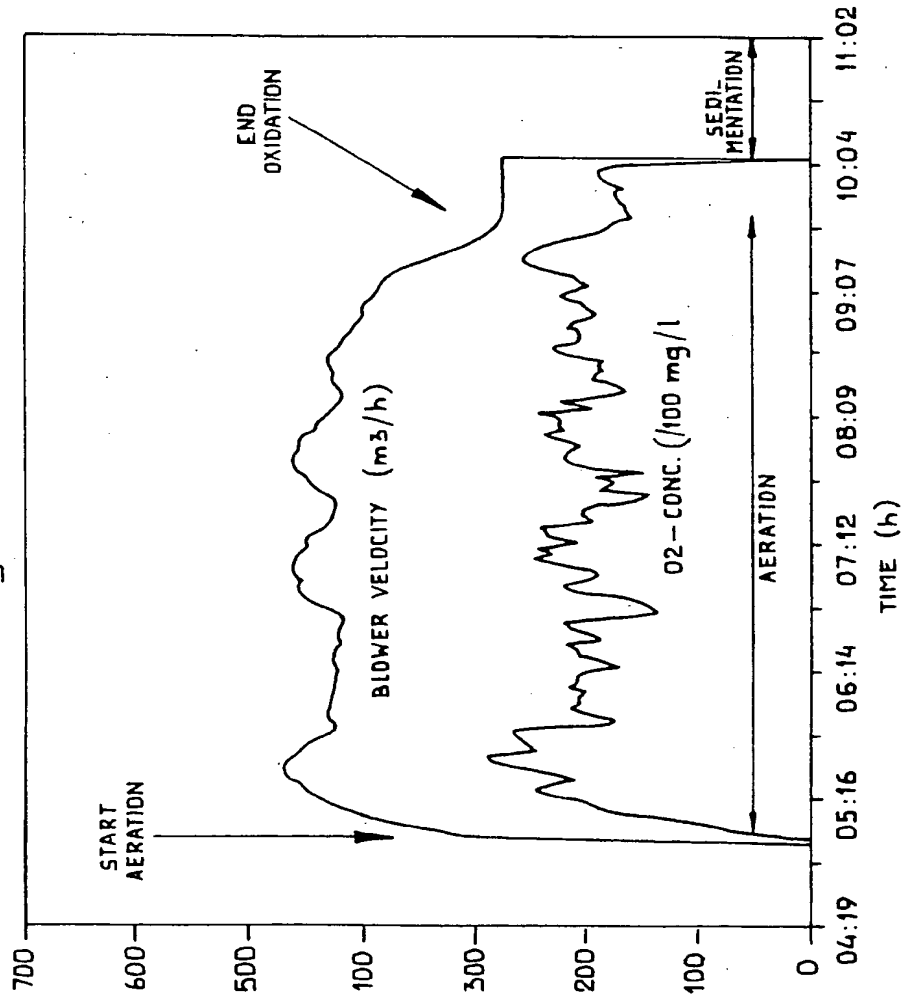


fig-18





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Page 1

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Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.5)
A	GB-A-2 099 807 (KUBOTA LTD) * page 2, line 59 - page 3, line 42; figure 3 * ---	1, 17, 18	C02F3/12
A	DE-A-3 932 640 (ORPEGEN MEDIZINISCH-MOLEKULARBIOLOGISCHE FORSCHUNGSGESELLSCHAFT) * claim 1 * ---	8	
A	WATER SCIENCE AND TECHNOLOGY vol. 13, no. 9, 1981, OXFORD-GB pages 233 - 238; U. PAGGA AND W. GÜNTNER: 'The BASF toxinometer - a helpful instrument to control and monitor biological waste water treatment plants' * page 234 * ---	1	
A	EP-A-0 327 184 (GIST-BROCADES) * figure 1 * ---	8	
A	DE-A-3 605 962 (STADTWERKE VIERSEN) * abstract * ---	1	
A	ABWASSESTECHNIK vol. 38, no. 4/88, 1988, WIESBADEN-DE pages 12 - 16; J. BRUNS: 'Steuerungskonzepte bei der vorgeschalteten denitrifikation' * the whole document * ---	1	TECHNICAL FIELDS SEARCHED (Int. Cl.5)
A	PATENT ABSTRACTS OF JAPAN vol. 13, no. 137 (C-582)5 April 1989 & JP-A-63 302 996 (EBARA INFILCO) 9 December 1988 * abstract * ---	1	C02F
A	PATENT ABSTRACTS OF JAPAN vol. 4, no. 34 (C-3)22 March 1980 & JP-A-55 008 852 (EBARA INFILCO) 22 January 1980 * abstract * ---	1	
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 02 JANUARY 1992	Examiner KASPERS H.M.C.
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Page 2

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A	PATENT ABSTRACTS OF JAPAN vol. 5, no. 114 (C-64)23 July 1981 & JP-A-56 053 795 (EBARA INFILCO) 13 May 1981 * abstract * ---	1	
A	PATENT ABSTRACTS OF JAPAN vol. 7, no. 195 (C-183)25 August 1983 & JP-A-58 098 195 (HITACHI SEISAKUSHO) * abstract * ---	1	
A	PATENT ABSTRACTS OF JAPAN vol. 5, no. 114 (C-64)23 July 1981 & JP-A-56 053 795 (EBARA INFILCO) 13 May 1981 * abstract * ---	1	
A	PATENT ABSTRACTS OF JAPAN vol. 4, no. 34 (C-3)22 March 1980 & JP-A-55 008 852 (EBARA INFILCO) 22 January 1980 * abstract * ---	1	
A	H. SPANJERS & A. Klapwijk 'On-line meter for respiration rate and short-term biochemical oxygen demand in the control of the activated sludge process'. PROC. 5th IAWPRC WORKSHOP ON & INSTRUMENTATION, CONTROL AND AUTOMATION, Yokohama/Kyoto, page 67-77 -----	1,11	TECHNICAL FIELDS SEARCHED (Int. Cl.5)
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 02 JANUARY 1992	Examiner KASPERS H. M. C.
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